

## A P P E N D I X I:

THE LISTING OF CLAIMS (version with markings, showing the changes made):

1. (currently amended) A process for working up solutions of hydroxylamine and amines, wherein the hydroxylamine is stripped [~~from~~] from the hydroxylamine-containing solution with steam.
2. (currently amended) A process as claimed in claim 1, wherein the solution is passed into a rectification column and the hydroxylamine is stripped by the countercurrent method with steam, with a top product comprising aqueous hydroxylamine and a bottom product comprising amines being obtained. 7.43
3. (~~canceled~~) ~~A process as claimed in claim 2, wherein the top product is condensed and is partly recycled to the rectification column, with a reflux ratio of less than 0.5.~~
4. (previously amended) A process as claimed in claim 2, wherein the rectification column is operated at from 0.1 to 1.0 atmosphere.
5. (original) A process as claimed in claim 2, wherein some of the bottom product <sup>is</sup> vaporized again<sup>u</sup> by means of an evaporator and <sup>the</sup> vaporous fractions<sup>u</sup> are recycled to the rectification column. CA  
in process
6. (previously amended) A process as claimed in claim 2, wherein water is added to the liquid phase<sup>u</sup> of the rectification column.
7. (previously added) A process as claimed in claim 4, wherein the rectification column is operated at from 0.8 to 1.0 atmosphere.
8. (previously added) A process as claimed in claim 6, wherein the water is passed into the bottom of the rectification column.
9. (previously added) A process as claimed in claim 1, wherein the solution is from the electronics industry.
10. (new) A process for working up a solution of hydroxylamine and amines,  
wherein the hydroxylamine is stripped from the hydroxylamine-containing solution with steam,  
wherein the solution is passed into a rectification column and steam is passed counter-currently through the column, whereby a top product comprising aqueous hydroxylamine and a bottom product comprising amines are obtained, and 7.97.

wherein the top product is condensed and is partly recycled to the rectification column with a reflux ratio of less than 0.5.

11. (new) A process as claimed in claim 10, wherein the rectification column is operated at from 0.1 to 1.0 atmosphere.
  12. (new) A process as claimed in claim 11, wherein the rectification column is operated at from 0.8 to 1.0 atmosphere.
  13. (new) A process as claimed in claim 10, wherein some of the bottom product is vaporized again by means of an evaporator and the vaporous fractions are recycled to the rectification column.
  14. (new) A process as claimed in claim 10, wherein water is added to the liquid phase of the rectification column.
  15. (new) A process as claimed in claim 14, wherein the water is passed into the bottom of the rectification column.
  16. (new) A process as claimed in claim 10, wherein the solution is from the electronics industry.
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## A P P E N D I X II:

THE AMENDED CLAIMS (clean version of all claims):

1. (currently amended) A process for working up solutions of hydroxylamine and amines, wherein the hydroxylamine is stripped from the hydroxylamine-containing solution with steam.
2. (currently amended) A process as claimed in claim 1, wherein the solution is passed into a rectification column and the hydroxylamine is stripped by the countercurrent method with steam, with a top product comprising aqueous hydroxylamine and a bottom product comprising amines being obtained.
4. (previously amended) A process as claimed in claim 2, wherein the rectification column is operated at from 0.1 to 1.0 atmosphere.
5. (original) A process as claimed in claim 2, wherein some of the bottom product is vaporized again by means of an evaporator and the vaporous fractions are recycled to the rectification column.
6. (previously amended) A process as claimed in claim 2, wherein water is added to the liquid phase of the rectification column.
7. (previously added) A process as claimed in claim 4, wherein the rectification column is operated at from 0.8 to 1.0 atmosphere.
8. (previously added) A process as claimed in claim 6, wherein the water is passed into the bottom of the rectification column.
9. (previously added) A process as claimed in claim 1, wherein the solution is from the electronics industry.
10. (new) A process for working up a solution of hydroxylamine and amines,  
wherein the hydroxylamine is stripped from the hydroxylamine-containing solution with steam,  
wherein the solution is passed into a rectification column and steam is passed counter-currently through the column, whereby a top product comprising aqueous hydroxylamine and a bottom product comprising amines are obtained, and  
wherein the top product is condensed and is partly recycled to the rectification column with a reflux ratio of less than 0.5.

11. (new) A process as claimed in claim 10, wherein the rectification column is operated at from 0.1 to 1.0 atmosphere.
12. (new) A process as claimed in claim 11, wherein the rectification column is operated at from 0.8 to 1.0 atmosphere.
13. (new) A process as claimed in claim 10, wherein some of the bottom product is vaporized again by means of an evaporator and the vaporous fractions are recycled to the rectification column.
14. (new) A process as claimed in claim 10, wherein water is added to the liquid phase of the rectification column.
15. (new) A process as claimed in claim 14, wherein the water is passed into the bottom of the rectification column.
16. (new) A process as claimed in claim 10, wherein the solution is from the electronics industry.